



AN ECONOMICAL/ENVIRONMENTAL PROPOSED SOLUTION FOR REUSING THE FLARE ASSOCIATED GASES IN RAS-GHARIB OIL FIELDS

By

Mostafa Mohamed Samy Mostafa

A Thesis Submitted to the
Faculty of Engineering at Cairo University
in Partial Fulfillment of the
Requirements for the Degree of
MASTER OF SCIENCE
in
Chemical Engineering

FACULTY OF ENGINEERING, CAIRO UNIVERSITY
GIZA, EGYPT
2016





AN ECONOMICAL/ENVIRONMENTAL PROPOSED SOLUTION FOR REUSING THE FLARE ASSOCIATED GASES IN RAS-GHARIB OIL FIELDS

By Mostafa Mohamed Samy Mostafa

A Thesis Submitted to the
Faculty of Engineering at Cairo University
in Partial Fulfillment of the
Requirements for the Degree of
MASTER OF SCIENCE
in
Chemical Engineering

Under the Supervision of

Prof. Dr. Fatma Elzahraa Hanafy Ashour

Dr. Mamdouh Ayad Gadallah

Professor of Chemical Engineering Head manager of Chemical Engineering Dept. Faculty of Engineering, Cairo University Professor Assistant of Chemical Engineering Chemical Engineering Dept. Faculty of Engineering, British University in Egypt

FACULTY OF ENGINEERING, CAIRO UNIVERSITY
GIZA, EGYPT
2016





AN ECONOMICAL/ENVIRONMENTAL PROPOSED SOLUTION FOR REUSING THE FLARE ASSOCIATED GASES IN RAS-GHARIB OIL FIELDS

By Mostafa Mohamed Samy Mostafa

A Thesis Submitted to the
Faculty of Engineering at Cairo University
in Partial Fulfillment of the
Requirements for the Degree of
MASTER OF SCIENCE
in
Chemical Engineering

Approved by the:

Prof. Dr. Nabil Mahmoud Abd El-Monem Chemical Engineering Department, Cairo University

Prof. Dr. Fatma Elzahraa Hanafy Ashour Chemical Engineering Department, Cairo University

Prof. Dr. Attia Mahmoud Attia Petroleum Engineering Department, British University in Egypt

Dr. Mamdouh Ayad Gadallah Chemical Engineering Department, British University in Egypt

FACULTY OF ENGINEERING, CAIRO UNIVERSITY GIZA, EGYPT

Engineer's Name: Mostafa Mohamed Samy Mostafa

Date of Birth: 04/08/1987 Nationality: Egyptian

E-mail: mostafasamy_87@hotmail.com

Phone: 01022115298

Address: 7th Emad El-Deen Kamel Street – Nasr-City - Cairo

Registration Date: 01/03/2011

Awarding Date: 2016 Degree: Master of Science.

Department: Chemical Engineering Department

Supervisors:

Prof. Dr. Fatma Elzahraa Hanafy Ashour Prof. Ass. Dr. Mamdouh Ayad Gadallah

Examiners:

Prof. Dr. Nabil Mahmoud Abd El-Monem Chemical Engineering Department, Cairo University Prof. Dr. Fatma Elzahraa Hanafy Ashour Chemical Engineering Department, Cairo University

Prof. Dr. Attia Mahmoud Attia

Petroleum Engineering Department, British University in Egypt

Dr. Mamdouh Ayad Gadallah

Chemical Engineering Department, British University in Egypt

Title of Thesis:

AN ECONOMICAL/ENVIRONMENTAL PROPOSED SOLUTION FOR REUSING THE FLARE ASSOCIATED GASES IN RAS-GHARIB OIL FIELDS

Key Words:

Flared associated gas, sweetening process, Valuable products.

Summary:

The General Petroleum Company produces about 40,000 barrels of crude oil daily from Ras-Gharib concession, with this quantity of crude oil there are 22 MMSCFD of associated gases. A part of this gas flow, which is approximately 7MMSFCD, is injected directly to injection wells to maintain the reservoir pressure. The rest, i.e. 15 MMSCFD of these associated gases, is transmitted directly to the flare from El-Hamd, Gharib and Fanar fields. The current research work proposes a solution to reuse the raw associated gases produced in Ras-Gharib into a valuable material and consequently addressing the above environmental/societal implications. This study performs economic and environmental evaluations accounting for the profitability, revenues and economics of treating these raw associated gases in a sweetening unit to produce sweet gas and hydrogen sulfide that minimize carbon monoxide and carbon dioxide emissions.



ACKNOWLEDGMENTS

I provide my acknowledgments to all people who gave and still give their support. I have to thank **Prof. Dr. Fatma El-Zahraa Ashour, Prof. Dr. Nabil Mahmoud Abd El-Monem, Prof. Dr. Attia Mahmoud Attia** and **Prof. Ass. Dr. Mamdouh Gadallah** for providing me with very precious advices and ideas for all the sections inside this master study that helped me a lot bringing out the best of me.

I wish to send a special award to the spirit of my mother *Mrs. Iglal Ibrahim Badawy* as i miss her at this time.

I especially want to express my sincere gratitude to my parents *Mr. Mohamed Samy Mostafa,Mrs. Fahima Ali Abd El-wahed, Mr. Mohamed Abd El-Halim El-Hosiny and Mrs. Omaima Ahmed Tawfeek* who gives me a great support in my work and my life.

My deepest gratitude to my wife *Mrs. Maha Abd El-Halim El-Hosainy* for believing in me, encouraging me to complete this thesis and beat the barriers.

TABLE OF CONTENTS

ACKNOWLEDGMENTS	
TABLE OF CONTENTS	
LIST OF TABLES	
LIST OF FIGURES	
ABBREVIATIONABSTRACT	
ADSTRACT	V 111
CHAPTER 1: INTRODUCTION	1
CHAPTER 2: LITERATURE REVIEW	3
2.1. INTRODUCTION	
2.2. NATURAL GAS TREATING	
2.2.1. Hydrogen sulfide (H2S)	
2.3. APPLIED GAS SWEETENING PROCESSES	
2.3.1. Adsorption processes	
2.3.1.2. Properties for adsorbents	
2.3.2. Absorption processes	
2.3.3. Types of Absorption processes9	
2.3.3.1. Absorption processes using a regenerative chemical reaction	
2.3.3.2. Equipment for absorption	
2.3.4. Process selection	
2.3.5. Selection of flow type	
2.4.1 Types of amines	
2.5. DESIGN PROCEEDINGS FOR AMINE SWEETENING SYSTEMS	
2.6. ABSORPTION TOWER DESIGN	
2.6.1 Determination of amine solution flow rates.	
2.6.2. Determination of number of plates graphically	
2.6.3. Diameter determination.	
2.6.4. Height determination	
2.6.5. Regeneration tower design	
2.7. PROCESS SIMULATION BY USING HYSYS	
2.8. ECONOMIC EVALUATION FOR THE PROPOSED SWEETENING PLANT	
2.8.1. Types of cost estimation	
2.8.1.1. Analogous estimation	
2.8.1.2. Parametric estimation.	
2.8.1.3. Three-point estimating.	
2.8.2. Design of cost analysis	
2.8.2.1. Capital expenditure	
2.8.2.2. Operating cost	
2.8.2.2.1. Fixed costs	
2.8.2.2.2. Variable costs	32

2.8.3. Cost escalation.	
2.8.4. Rate of return	33
CHAPTER 3: PROBLEM STATEMENT AND OBJECTIVE OF THE RESEAL	RCH35
CHAITERS, INCODED, I STATE WILL AND CONCESTIVE OF THE RESERVE	
3.1. RAS-GHARIB CONCESSION	36
3.2. PROBLEM STATEMENT	37
3.2.1. Environmental impact	37
3.2.2. Economic impact	
3.3. PROPSED SOLUTION FOR REUSING THE FLARE ASSOCIATED GAS	
CHAPTER 4: CASE STUDY AND RESULTS	41
4.1. SOLVENT SELECTION	41
4.1.1. Suitable solvents for this case study	47
4.2. AMINE SOLUTION SELECTION CRITERIA	
4.2.1. Determination of amine solutions flowrate	50
4.2.2. Different amines flow rate calculated by using software program	52
4.3. ABSORPTION TOWER DESIGN	
4.3.1. Type of absorption tower	56
4.3.2. Determination of number of tower plates	56
4.3.3. Absorber diameter determination	
4.3.4. Determination of absorption tower height	61
4.4. PLANT SETTING UP BY USING HYSYS	61
4.4.1. Feed streams inlet temperature to the absorber tower	66
4.4.2. Concentration diagram for the absorber tower	68
4.4.3. Effect of equilibrium constant	69
4.4.4. Effect of increasing pure amine flowrate on H2S content	72
4.5. COST ESTIMATION FOR THE SIMULATED SWEETENING PLANT	73
4.5.1. Capital cost	73
4.5.1.1. Estimation of purchased equipment cost	73
4.5.1.2. Piping, instrumentation and electrical costs	74
4.5.2. Chemical engineering plant cost index	74
4.5.3. Operating costs	75
4.5.3.1. Fixed costs	75
4.5.3.2. Variable costs	75
4.5.4. Economic evaluation of this unit	76
CONCLUSION	77
REFERENCES	79

LIST OF TABLES

Table 2.1: The composition of natural gas	5
Table 2.2: Symptoms from exposure to H2S	6
Table 2.3: Physical characteristics for some adsorbents	8
Table 2.4: Advantages and disadvantages for the used absorption towers	14
Table 2.5: Required values for amine flow rate determination	21
Table 2.6: The assumed K-value for the three amines	23
Table 2.7: Estimation factors of capital cost for plant	31
Table 2.8: Cost of utilities used in gas plants in 2004	32
Table 3.1: Flared gas quantity for each field	37
Table 4.1: Fanar filed composition	42
Table 4.2: Gharib field composition	43
Table 4.3: El- Hamd field composition	
Table 4.4: The combined feed stream calculated by using HYSYS	45
Table 4.5: Optimum MEA flowrate data	
Table 4.6: Optimum DEA flowrate data	51
Table 4.7: Optimum MDEA flowrate data	
Table 4.8: The price per ton for each amine solvent	51
Table 4.9: The optimum flow rate for each amine lean solution with its cost	56
Table 4.10: The calculated number for absorption tower plates	57
Table 4.11: Composition for the three solutions	58
Table 4.12: Estimation of purchased equipment cost based on year 2004	

LIST OF FIGURES

Figure 2.1: Typical process operation units in a gas plant	3
Figure 2.2: Methods for gas sweetening	7
Figure 2.3: A spray tower	10
Figure 2.4: A tray tower	
Figure 2.5: An example of a tray with structure packing	
Figure 2.6: Example of elements for random packing	
Figure 2.7: A venturi absorber	
Figure 2.8: Selection of gas-sweetening processes by H2S content	
Figure 2.9: Selection of gas-sweetening processes by H2S partial pressure	
Figure 2.10: The different types of amines	
Figure 2.11: Amine system for gas sweetening	
Figure 2.12: Absorption tower stage calculations	
Figure 2.13: The number of plates of absorption tower	
Figure 2.14: Operating conditions for absorption tower	
Figure 2.15: Operating conditions for regeneration tower	
Figure 2.16: Sweetening process simulation flowsheet model	
Figure 2.17: Cost evaluation mechanism	
Figure 2.18: Cost of vertical vessel in 2004.	
Figure 2.19: Cost of tower plates in 2004.	
Figure 2.20: Cost of sell and tube heat exchanger in 2004.	
Figure 3.1: GPC petroleum concessions	
Figure 3.3: Ras-Gharib concession fields	
Figure 3.4: Flare in Ras-Gharib city	
Figure 3.5: Flare associated gases path from Ras-Gharib fields	
Figure 3.6: Proposed solution for reusing the flare associated gases in Ras-G	
concession	
Figure 4.1: The objective of the research work	
Figure 4.2: Selection of optimum solvent by for this case study	
Figure 4.3: Selection of optimum solvent by using H2S partial pressure	
Figure 4.4: Physical solvents sweetening plant	
Figure 4.5: Two-stage mixed solutions sweetening plant	
Figure 4.6: Sweetening absorber	52
Figure 4.7: Hydrogen sulfide rate for MEA solution flow rate	
Figure 4.8: Hydrogen sulfide rate for DEA solution flow rate	53
Figure 4.9: Hydrogen sulfide rate for MDEA solution flow rate	53
Figure 4.10: Relation between 20% MEA flow rate and both H2S removal and	
cost	54
Figure 4.11: Relation between 30% DEA flow rate and both H2S removal and	flow
cost	
Figure 4.12: Relation between 50% MDEA flow rate and both H2S removal and	flow
cost	
Figure 4.13: McCabe Thiele diagram using MEA solution	
Figure 4.14: McCabe Thiele diagram using DEA solution	
Figure 4.15: McCabe Thiele diagram using MDEA solution	
Figure 4.16: McCabe Thiele comparison for the three cases	
Figure 4.17: MEA 20% solution sweetening simulation unit	63

Figure 4.18: DEA 30% solution sweetening simulation unit	64
Figure 4.19: MDEA 50% solution sweetening simulation unit	65
Figure 4.20: Relation between lean MEA inlet temperature to the H2S content in	the treated
product	66
Figure 4.21: Relation between lean DEA inlet temperature to the H2S content in product	the treated
Figure 4.22: Relation between lean MDEA inlet temperature to the H2S content in product	the treated
Figure 4.23: Relation between sour gas inlet temperatures to absorption tower fo amine solutions	
Figure 4.24: Acid gas composition in the absorber using MEA	
Figure 4.25: Acid gas composition in the absorber using DEA	68
Figure 4.26: Acid gas composition in the absorber using MDEA	69
Figure 4.27: K-values-Temperature relation for MEA	70
Figure 4.28: K-values-Temperature relation for DEA	71
Figure 4.29: K-values-Temperature relation for MDEA	71
Figure 4.30: Effect of MEA flowrate variation on H2S content	72
Figure 4.31:Effect of DEA flowrate variation on H2S content	72
Figure 4.32: Effect of MDEA flowrate variation on H2S content	73

ABBREVIATION

LNG Liquefied natural gas
LPG Liquefied petroleum gas

MMSCFD Million standard cubic feet per day

BBL Barre

GPC The general petroleum company

COS Carbonyl sulfide
MF Mole fraction
PPM Part per million
GPM gram per minute
MM milli-meter

CAPEX
OPEX
OPEX
Operating costs
RBLR Q
COND Q
Condenser heat duty

USA The united states of America

US \$ United states dollar

°R Radian

MEAMono-ethanol amineDEADi-ethanol amineMDEAMethyl di-ethanol amine

XEA Amine solution

ABSTRACT

The General Petroleum Company "GPC" is an Egyptian company in the field of oil and gas production that owns a Petroleum Concession in Ras-Gharib City in the Eastern Desert in Egypt. GPC produces about 40,000 barrels of crude oil daily from Ras-Gharib concession, with this quantity of crude oil there are 22 MMSCFD of associated gases. A part of this gas flow, which is approximately 7MMSFCD, is injected directly to injection wells to maintain the reservoir pressure. The rest, i.e. 15 MMSCFD of these associated gases, is transmitted directly to the flare from El-Hamd, Gharib and Fanar fields.

In addition to being a waste of valuable materials, the transmitted associated gases to flares impose huge environmental problems to Ras-Gharib city as this stream of gases contains acid gas content exceeding 13 mol % (10.45% H₂S and 3.24 % CO₂). Further, there are some societal implications in the region due to the flaring, such as Nausea and vomiting, Kidney failure, Sterility, Lung Cancer, and Blindness. Also, carbon monoxide and carbon dioxide gases are emitted to the atmosphere with additional environmental impact.

The current research work proposes a solution to reuse the raw associated gases produced in Ras-Gharib into a valuable material and consequently addressing the above environmental/societal implications. This study performs economic and environmental evaluations accounting for the profitability, revenues and economics of treating these raw associated gases in a sweetening unit to produce sweet gas and hydrogen sulfide that minimize carbon monoxide and carbon dioxide emissions. Furthermore, H₂S can be processed to produce free sulfur to minimize pollution totally. The designed treatment process conforms to the international H₂S contents in the sweet natural gas as 4 ppm in the sales gas. The research study includes several tasks, such as selecting the optimum sweetening process (amine solutions), minimizing the hydrogen sulfide content, and optimizing the operating conditions. A potential economical added value of the proposed solution implies that the sweet gas produced can be pumped directly into the Egyptian National Network for Gas. Furthermore, Liquefied Petroleum Gas can be obtained from this sweet gas, while elemental sulfur can be obtained in a sulfur recovery unit.

The proposed processing unit provides sales gas into the local Egyptian network of capacity of 10 MMSCFD, equivalent to some 2000 barrels/day of petroleum crude oil. The economics of the treatment unit results in an annual net profit of 2.3 million Dollars. The capital costs of the proposed project are estimated as 10 million Dollars, including the initial costs of the amine solutions. The rate of return for the project in the first year is 100 % with a payback time of one year.

CHAPTER 1: INTRODUCTION

Natural gas is a combustible mixture of hydrocarbon gases and other impurities. The natural gas industry was started in the beginning of the twentieth century in the United States. This industry produces high quality fuel as it considered one of the cleanest fuel sources all over the world. Besides that, many valuable petroleum chemicals produced from this industry. Raw natural gas is found in deep reservoirs underground. This raw natural gas occurs either in association with crude oil as it named associated gas or dry gas without crude oil which named non-associated gases. Although, this dry gas may contain large amount of natural gas liquids (NGL) components.

The General Petroleum Company "GPC" is an Egyptian company in the field of oil and gas production that has three concessions. Ras-Gharib concession one of these. It consists of 20 petroleum fields. In this concession, about 40,000 barrels of crude oil are produced daily. With this quantity of crude oil, there are 22 MMSCFD "million standard cubic feet per day" of associated gases produced. 7 MMSFCD are injected directly to injection wells to maintain the reservoir pressure. but the reminder which is 15 MMSCF daily are transmitted directly to the flare without any benefit but also with huge environmental pollution as this stream of gases it's acid gas content exceeds 13 mol %. These flared gas streams are produced from three fields (Gharib, Al-Hamd and Fanar).

These associated gases are produced in a city occupied with huge number of people as its population numbered 100,000. There are some societal implications in the region due to the flaring, such as Nausea and vomiting, Kidney failure, Sterility, Lung Cancer, and Blindness. Also, carbon monoxide and carbon dioxide gases are emitted to the atmosphere with additional environmental impact. Beside the huge environmental impact there is an economic impact for flaring these raw gas streams without any benefit. These flared gas streams can be treated to produce many valuable products such as: liquefied natural gas (LNG), liquefied petroleum gas (LPG), condensate, pure sulfur and sweet sales gas which can be either pumped to the Egyptian National Network for Gas or injected directly to injection wells to maintain the reservoir pressure as the rest. Minimizing Environmental pollution and harmful emissions saves a huge amount of money that spent to cure the caused clinical diseases in addition to the removal of the H2S.

The current research work proposes a solution to reuse the raw associated gases produced in Ras-Gharib into a valuable material and consequently addressing the above environmental/societal implications using simulating program in order to find the optimum conditions and process. This study performs economic and environmental evaluations accounting for the profitability, revenues and economics of treating these raw associated gases in a sweetening unit to produce sweet gas and hydrogen sulfide that minimize carbon monoxide and carbon dioxide emissions. Furthermore, H₂S can be processed to produce free sulfur to minimize pollution totally. The designed

treatment process conforms to the international H_2S contents in the sweet natural gas as 4 ppm in the sales gas.

The proposed processing unit provides sales gas into the local Egyptian network of capacity instead of flare these gases. This sales gas can be further processed to produce many valuable products. Condensate, Liquefied petroleum gas, butane and propane can be produced to add an economic value to the project. This project will minimize the harmful gas emissions hence, minimize clinical diseases caused in presence of harmful gas emissions. Besides that, hydrogen sulfide produced in the sweetening unit used that can be further processed in sulfur recovery unit to produce pure sulfur. This pure sulfur can be sold directly as it used in many industries as fertilizers.

CHAPTER 2: LITERATURE REVIEW

2.1. Introduction

Natural gas is defined as a composition of light hydrocarbons with a low content of heavy hydrocarbons. When the natural gas only contains these compounds it will be defined as a dry gas as it found in deep underground without crude oil or as a gas cap over crude oil. When the natural gas is found with crude oil it called associated gas. Raw natural gas stream must be processed before it can be transmitted into long-distance pipeline systems for consumers. The target of gas processing is to extract natural gas, condensate, acid gases, and water from the raw natural gas stream and condition each fluid of these for sale or disposal. The typical process operation units are summarized in figure 2.1. Each unit consists of a specific group of equipment performing a specific function together. All these units will not necessarily to be in every gas plant.

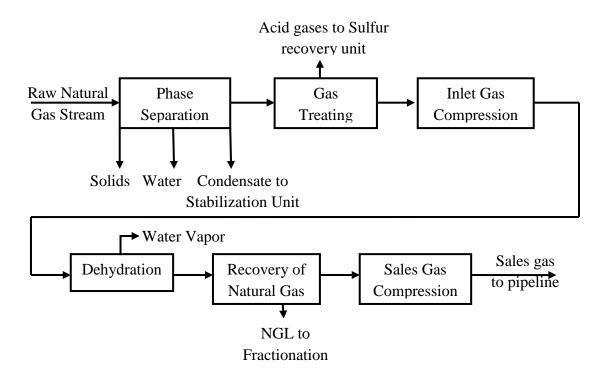


Fig 2.1: Typical process operation units in a gas plant [1]

The first unit is the phase separation of the different phases, which are gas, liquid hydrocarbons, liquid water, and/or solids. Phase separation of the production stream is mostly done in a slug catcher then in an inlet separator. The slug catcher is designed to separate gas, hydrocarbon condensate, and inlet water. Then the gas stream is sent to the inlet separator. Hydrocarbon condensate recovered from natural gas and may be shipped without further processing. Hydrocarbon condensate produced from the inlet