



NUMERICAL INVESTIGATION FOR HEAT TRANSFER ENHANCEMENT IN PARABOLIC TROUGH ABSORPTION TUBE USING TWISTED TAPE INSERTS

By

Mohamed Ahmed Abdelazim Abousabae

A Thesis Submitted to the
Faculty of Engineering at Cairo University
In Partial Fulfillment of the Requirements for the Degree of
MASTER OF SCIENCE
In
MECHANICAL POWER ENGINEERING

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Key Words:

Fluid Dynamics; Heat Transfer; Twisted Tape; Parabolic Trough Absorption Tube; Solar Energy

Summary:

In this work, the thermal performance of parabolic trough absorption tube with twisted tape inserts were analyzed numerically using ANSYS FLUENT 15.0 software. An optical modelling tool that uses Monte-Carlo ray tracing techniques (Soltrace) was used to obtain the non-uniform heat flux distribution on the parabolic trough absorber tube. The results show that the use of twisted tape inserts results in high heat transfer rates due to the increased turbulence intensity and the mixing of the heat transfer fluid from that part of the absorber tube which receive concentrated heat flux with the heat transfer fluid from the part which receive only direct solar heat flux and the heat transfer increases between 17 % and 84 % and friction factor increases between 117 % and 415 %



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NOMENCLATURE

Symbol	Quantity
K	Thermal conductivity, w/m.k
$A_{ap,r} \\$	Absorption tube aperture area, m ²
$A_{ap,c}$	Collector aperture area, m ²
L	Length of the trough, m
f	The focal length, m
a	The aperture width, m
C_{G}	Geometric concentration ratio
$d_{\rm ro}$	Absorption tube outer diameter, m
$d_{ri} \\$	Absorption tube inner diameter, m
$d_{gi} \\$	Glass cover inner diameter, m
d_{go}	Glass cover outer diameter, m
Nu	Nusselt number
Nuen	Nusselt number for enhanced absorber tube
Nu_p	Nusselt number for plain absorber tube
X	Thermal enhancement factor
Н	Twist tape pitch, m
W	Twist tape width, m
Y	Twist ratio
$T_{sky} \\$	Sky temperature, K
$h_{\rm w}$	Wind heat transfer coefficient, w/m ² .k
cp	Specific heat of fluid, J/kg.K
g _i Gk	The component of the gravitational vector in the i th direction, m/ s ² Turbulence kinetic energy generated due to the mean velocity gradients
K	Kinetic energy of turbulence, m ² /s ²
kp	Turbulence kinetic energy at point P, m ² /s ²
] D#	Length scale of Turbulence, m
Pr ġ	Molecular Prandtl number, $Pr = Cp \mu / k$ Wall heat flux, W/m^2
Su	The source term

Sφ	The source term
Ti	Inlet temperature, °C
Tp	Temperature at the cell adjacent to wall, °C
Tw	Temperature at the wall, °C
\vec{u}	The flow velocity vector, m/s
\vec{u}_g	The grid velocity of the moving mesh, m/s
u_{i}	The fluctuating velocity component, m/s
$\overline{u_i}$	The mean velocity component, m/s
$\mathbf{u}_{\mathbf{j}}$	Mean velocity component, m/s
U_{p}	Mean velocity of the fluid at point P , m/s
Y_{M}	The contribution of the fluctuating dilatation to the overall dissipation rate
У Р	Distance from point to the wall, m
y_T^*	The non-dimensional thermal sublayer thickness

Greek Letters

ρ	Density of the fluid, kg/m ³
$ au_{ij}$.	The stress tensor, N/m^2
ψ	Rim angle, degree
θ	Circumferential angle, degree
μ	Viscosity, kg/m.s
3	Emissivity,
δ_{ij}	Kronecker delta
$\mu_{\it eff}$	Effective turbulent viscosity
Γφ	The diffusion coefficient
μ_t	Turbulent viscosity, kg.m/s
ϵ	Turbulence dissipation rate, m ² /s ³
β	Coefficient of thermal expansion, K-1
δV_j	The volume swept out by the control volume face j
Φ_f	Value of Φ convected through face f
$ abla\Phi$	Gradient of Φ
σ_{ε}	The turbulent Prandtl numbers for ε
σ_{K}	The turbulent Prandtl numbers for k
$\rho \overline{u_i^{'}u_j^{'}}$	Reynolds stresses term

ABBREVIATIONS

CFD Computational Fluid Dynamics

CSP Concentrated Solar Power Plants

DNI Direct Normal Irradiance

EES Engineering Equation Solver

FVM Finite Volume Method

HCE Heat Collection Element

HTF Heat Transfer Fluid

IPH Industrial Heat Process

LCR Local Concentration Ratio

LVG Longitudinal Vortex Generators

MCRT Monte Carlo Ray Tracing Method

NREL National Renewable Energy Laboratory

PTC Parabolic trough Collector

RANS Reynolds Averaged Navier-Stokes equations

RKE Realizable K-ε Turbulence Model

RNG Re-normalization Group K-ε Turbulence Model

SNL Sandia National Laboratory

mtoe Million Tonnes of Oil Equivalent

ABSTRACT

Parabolic trough systems are one of the most commercially technologies for concentrated solar power. The main development efforts are concentrating on reducing the cost of this technology. The cost reduction options for parabolic trough systems include: (i) improving parabolic trough concentration ratio by increasing its sizes and (ii) improving the optical efficiency. However increasing the concentration ratio of parabolic trough system will cause more circumferential temperature difference on the absorption tube and will increase the system's thermal losses. So the development of the absorption tube becomes very important to increase the concentration ratio.

In the present work, the thermal performance of parabolic trough absorption tube with twisted tape inserts at different inlet temperatures, twist ratios and Reynolds numbers are investigated.

In this work, the thermal performance of parabolic trough absorption tube with twisted tape inserts is analyzed numerically by solving the governing equations using ANSYS FLUENT 15.0 software. An optical modelling tool that uses Monte-Carlo ray tracing techniques (Soltrace) was used to obtain the non-uniform heat flux distribution on the parabolic trough absorber tube. These heat flux distributions were then coupled to the CFD code as a boundary condition by using MATLAB code to convert them to a readable data by the profile function in ANSYS FLUENT 15.0 for the analysis of the thermal performance of the receiver.

The results show that the use of twisted tape inserts for heat transfer enhancement in parabolic trough receivers results in high heat transfer rates due to the increased turbulence intensity and the mixing of the heat transfer fluid from that part of the absorber tube which receive concentrated heat flux with the heat transfer fluid from the part which receive only direct solar heat flux. As the results demonstrated that the heat transfer increases between 17 % and 84 % while friction factor increases between 117 % and 415 % and thermal enhancement factor at a constant pumping comparison with a plain receiver tube was in the range 0.83 - 1.12. Also the results showed that the improved heat transfer performance in the absorption tube due to the use of twisted tape inserts reduces the absorption tube's circumferential temperature difference.