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شبكة المعلومات الجامعية التوثيق الالكتروني والميكروفيلم





جامعة عين شمس

التوثيق الإلكتروني والميكروفيلم قسم

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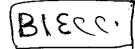


بالرسالة صفحات

لم ترد بالأصل



Menoufia University
Faculty of Electronic Engineering
Menouf



ADVANCED CONTROL METHOD APPLIED TO CEMENT INDUSTRY

A THESIS

Submitted for M. Sc. Degree in Automatic Control Engineering

By

MOHAMED HAMDY MOHAMED EL-SAYED

B. Sc. Automatic Control Engineering and Measurements Faculty of Electronic Engineering, Menoufia University

Approved by:

PROF. DR. TALAAT MOHAMED ABDEL-MONIEM

F 1 of Francisco

Faculty of Engineering

Alexandria University

PROF. DR. ESAM IBRAHIM EL-MADBOULY

Faculty of Electronic Engineering

Menoufia University

PROF. DR. MOHAMED IBRAHIM MAHMOUD

1 Mahman

Faculty of Electronic Engineering

Menoufia University

Menoufia University
Faculty of Electronic Engineering
Menouf

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Supervised by:

PROF. DR. ESAM I. EL-MADBOULY

Faculty of Electronic Engineering
Menoufia University

PROF. DR. MOHAMED NAGUIB HASSAN ALY

Faculty of Engineering

Alexandria University

PROF. DR. LAILA MOHI EL-DIN FARAG

[Laila Faray]
National Research Center

Cairo University

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MENOUFIA UNIVERSITY FACULTY OF ELECTRONIC ENGINEERING MENOUF

Abstract

A Master Thesis of

Advanced Control Method Applied to Cement Industry

By

Mohamed Hamdy Mohamed El-Sayed

(B.Sc.)

A mathematical model of heat transfer around the preheater tower in dry process in cement industry has been developed. A description of automatic control system of the preheater-kiln The model describes process by using fuzzy control is given. energy balance of each preheater stage. Relevant temperatures of the preheater tower (gas and dust) as well as those inside the cyclone (unmeasured) can be attained via this model. In addition, cyclone clogging diagnosis has been undertaken using two types of the advanced control. The first is the fuzzy controller which can reach the normal temperature values inside the cyclones with a minimum material feed. The second is the clog removal expert system which avoids the occurrence of clogging faults early. A dedicated expert diagnosis system presents to enhance the performance of the preheater tower by detecting the position of the prime clog early and select the proper solution to remove it by means of direct air cannons at the place of the prime clog only (not all cannons), and adjust the bypass ratio of the kiln gas automatically

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ABBREVIATIONS

SP Suspension preheater process

SF (Suspension preheater (SP) with Flash Furnace (FF)) process

SISO Single input-Single output system

FLC Fuzzy logic controller

CRES Clog Removal Expert System

LIST OF SYMBOLS

ε	Volatility of raw mix alkalis
V	Alkali valve =Bypass volume
K	Circulation factor
R _c	Residual content in the clinker
ΔQ_1	Heat carried in by fluid flow
ΔQ_1 ΔQ_2 ΔQ_3 ΔQ_4	Heat carried over to the next section
ΔQ_3	Heat transferred from the wall
ΔQ_4	Heat stored in the fluid
C	Heat capacitance of fluid per unit length
θ	Fluid temperature, assumed uniform in all transverse
	sections
v	Velocity of flow, assumed constant and uniform in a
	transverse section
R	Surface resistance per unit length
ϕ	Wall temperature
τ	Dimensionless time
η	Dimensionless distance
Ł	Total length of heat transfer line
L	Dead time
a	Dimensionless constant
C_h	Heat capacitance of a hot gas per unit length
C_c	Heat capacitance of a cold raw meal per unit length
\mathcal{O}_h	Velocity of hot gas phase inside gas duct and cyclone

U_c	Velocity of cold raw meal phase inside gas duct and cyclone
θ_h	Temperature of the hot gas phase
$ heta_{c}$	Temperature of the cold raw meal phase
L_h	Delay of the hot phase (gas)
L_c	Delay of the cold phase (raw meal)
a_h, a_c	Dimensionless constants
D	Time derivative in the nondimensional time domain $\partial / \partial t$
r	Delay ratio between two flows
$ heta_{{\scriptscriptstyle h}{\scriptscriptstyle 1}}$	Gas temperature inlet
$ heta_{c1}$	Raw meal temperature inlet
$ heta_{\scriptscriptstyle h2}$	Gas temperature outlet
$ heta_{c2}$	Raw meal temperature outlet
m_{feed}	Rate of raw meal feed
T_{gi}	Gas temperature outlet from cyclone (i)
T_{di}	Raw meal temperature outlet from cyclone (i)
K_{g}	Gain of the first order system
T_{g}	Time constant
E_{in}	Input energy
E_{out}	Input energy
m	Mass flow rate of the material
C_p	Specific heat of the material
K_i	Fraction value for each cyclone stage
$(m_x)_i$	Mass of the mixture inside cyclone i
$(C_{px})_i$	Specific heat of the mixture inside cyclone i
$(T_x)_i$	Temperature of the mixture inside cyclone i
$(m_g)_i$	Mass of the gas exit from cyclone i
$(C_{pg})_i$	Specific heat of the gas exit from cyclone i
$(m_d)_i$	Mass of the raw feed exit from cyclone i
$(C_{pd})_i$	Specific heat of the raw feed exit from cyclone i

i	Integer number = $1, 2,, 7$
T_{ref}	Reference temperature
Е	Error between the desired and process O/P
CE	Change of error between two samples
$U_{\mathbf{f}}$	Fuzzy value of rate of feed
U _o	Crisp value of rate of feed
T_{out}	Output temperature
$\mu_c(u)$	Membership function
V1	Preheater valve
V2	By-pass valve

LIST OF FIGURES

Fig.2.1	The section of quarry
Fig.2.2	Titan hummer crusher
Fig.2.3	Double rotor mill
Fig.2.4	Two double-deck silos
Fig.2.5	Preheater-Kiln system
Fig.2.6	Clinker Cooler
Fig.2.7	Various preheater kilns with their fuel energy requirements
Fig. 2.8	Suspension preheater and rotary kiln
Fig.2.9	Gas and material temperature of the individual stages of
:	cyclone preheater
Fig.2.9	Gas and material temperature of the individual stages of
	cyclone preheater
Fig. 2.10	Diagram of clinker burning process
Fig. 2.11	Krupp Polysius-Precalciner
Fig. 2.12	By-Pass installation in the kiln-preheater system
Fig. 2.13	Bypass reduction of the alkalis in clinker
Fig. 2.14	The definitions of concept
Fig. 2.15	The circulating factor
Fig.3.1	Cyclone preheater tower
Fig.3.2	Cyclone view
Fig.3.3	Heat percolation process
Fig.3.4	Parallel heat flow exchanger
Fig.3.5	Parallel heat flow exchanger solution
Fig.3.6	Block diagram of any cyclone (i) in the Preheater system
Fig.3.7	Block diagram of whole Preheater system