

بسم الله الرهكن الرّحيم

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تم رفع هذه الرسالة بواسطة /صفاء محمود عبد الشافي

بقسم التوثيق الإلكتروني بمركز الشبكات وتكنولوجيا المعلومات دون

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ADSORPTION OF COPPER AND ZINC FROM AQUEOUS SOLUTIONS USING FULLER'S EARTH: KINETICS, EQUILIBRIUM, AND THERMODYNAMICS

By

Ahmed Ali Ibrahim Eita

A Thesis Submitted to the
Faculty of Engineering at Cairo University
in Partial Fulfillment of the
Requirements for the Degree of
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in
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Under the Supervision of

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Title of Thesis:

Adsorption of Copper and Zinc from Aqueous Solutions Using Fuller's Earth: Kinetics, Equilibrium, and Thermodynamics

Kev Words:

Adsorption; Fuller's Earth; Copper; Zinc; Wastewater.

Summary:

Heavy metals are non-biodegradable toxins that can accumulate in nature. Many of the most widespread heavy metals are copper and zinc. Adsorption is an effective method for the uptake of heavy metals from wastewater. Thus, this research aimed to study the adsorption of copper and zinc onto fuller's earth. The effects of the solution's pH and initial concentration were investigated. The results showed that the efficiency of removal increased with the initial pH value of the solution. The optimum initial concentration of either copper or zinc for maximum removal efficiency was found to be 100 mg/L. The adsorption kinetics and mechanism were studied using pseudo-first-order, pseudosecond-order, Elovich equation, intra-particle, and Boyd models. The data were best fitted with a pseudo-second-order kinetic model for either copper or zinc concentrations. The data were also fitted using several isotherms for equilibrium studies, such as Langmuir, Dubinin-Radushkevich, Freundlich, and Temkin. The adsorption of either copper or zinc using fuller's earth was best fitted with a Dubinin-Radushkevich and Temkin isotherm, respectively. Thermodynamics and desorption studies were also reported. The results indicate that the adsorption efficiency increased with temperature, while desorption studies showed that HCl was able to regenerate the used fuller's earth. Finally, the morphology of the fuller's earth before and after adsorption was examined and showed the difference between the surfaces of fuller's earth before and after adsorption process.



Disclaimer

I hereby declare that this thesis is my own original work and that no part of it has been submitted for a degree qualification at any other university or institute.

I further declare that I have appropriately acknowledged all sources used and have cited them in the references section.

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Signature:

Acknowledgments

First and foremost, I am thankful to **Allah the Almighty God** for his grace and generosity.

I am extremely grateful to **Assoc. Prof. Dr. Minerva Edward Matta**, Associate Professor of Sanitary & Environmental Engineering, Cairo University, for her valuable assistance, continuous encouragement, and her advice during this work.

I am also extremely grateful to **Assoc. Prof. Dr. Safwat Mahmoud Safwat**, Associate Professor of Sanitary & Environmental Engineering, Cairo University, for his enormous help in developing this research idea, his helpful guidance, valuable assistance, continuous encouragement, and his advice during this work.

In addition, I am very grateful to **all my professors and teachers** who offered me a chance to expand my horizon and develop a better thinking mentality through different MSc courses.

Furthermore, I am very grateful to my **father and mother also my Family** for their continuous encouragement to finish this thesis in minimal time and their continuously moral support during this work.

Finally, I am grateful to my **Wife** for her continuous support and encouragement to finish this thesis.

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Nomenclature

2,4-DCP 2,4-dichlorophenol

A_{ad} surface area per gram of adsorbent

AC activated carbon

A_T Temkin isotherm equilibrium binding constant B Temkin constant related to heat of sorption

b_A Langmuir adsorption constant
B_{DR} Dubinin–Radushkevich constant

B_t the function of F

b_T Temkin isotherm constant C Constant in the isotherm models

C_{desorbed} the metal concentration liquid phase present in the desorbing solution

CdS Cadmium sulfide

C_e adsorbate equilibrium concentration in aqueous solution

CeO₂ Ceric oxide

C_o adsorbate initial concentration in aqueous solution

Conc. Concentration

Cu Copper

CuSO₄ Copper sulfate
Da Dalton unit

D_i effective diffusion coefficient

E adsorption energy

e⁻/h⁺ Suppressed recombination of photogenerated electrons/holes

EC electrocoagulation

EDX Energy Dispersive X-Ray Analysis EMRA Egyptian Mineral Resources Authority

EO electro-oxidation

EPA Environmental Protection Agency

ER electroreduction

F fractional attainment of equilibrium at different time t

FE Fuller's earth
HCl hydrochloric acid
J/mol Joule per mole

J/mol/K Joule per mole kelvin

K.V. kilovolt

K₁ constant for the Pseudo-first-order equation

K₂ rate constant for the Pseudo-second-order equation

 K_{ad} Langmuir adsorption equilibrium constant K_F Freundlich adsorption capacity parameter

K_{id} expression rate kJ/mol kilojoule per mole

M the reductant metal in cementation process

mol Mole

m²/g square meter per gram

MW molecular weight of adsorbate

N the noble metal in cementation process n Freundlich adsorption intensity parameter