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لم ترد بالأصل



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Electrodeposition of Copper Metal In Presence Of Surface Active Substances

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A Thesis

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(Chemistry)

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قد قبل للنشر . وسيشرف في العدد
الطبع في القريب العاجل .

وإني إذ أشكر سيادتكم كريم تعاونكم أرجو أن تتفضلوا بقبول وافر الاحترام .

مكتبة التحرير

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تحريراً في ١ / ١ / ١٩٨٧

بِسْمِ اللَّهِ الرَّحْمَنِ الرَّحِيمِ

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Nomenclature:

C_e interfacial concentration, mol/cm³

C_o bulk concentration, mol/cm³.

D diffusion coefficient of the metal ions, cm²/sec.

F faraday's constant = 96489 coulomb = 96489 A.sec.

Fr Froude number, $Fr = \frac{V^2}{hg}$.

g gravitational acceleration, cm/sec⁻².

h cathode height, cm.

V oxygen gas discharge velocity, cm/sec.

Gr Grashoff number, $Gr = \frac{g \alpha (C_o - C_e) l^3}{\nu^2}$.

I applied current, A.

i current density, A/cm².

i_l mean limiting current density averaged over the whole electrode surface, A/cm²

J mass transfer rate excluding migration, mol/cm².sec.

K equilibrium constant of the adsorption reaction.

k mass transfer coefficient, cm/sec.

P atmospheric pressure.

Re Reynolds number, $Re = \frac{Ul}{\nu}$.

Sc Schmidt number, $Sc = \frac{\nu}{D}$.

Sh Sherwood number, $Sh = \frac{kl}{D}$.

T absolute temperature, K.

z the number of transferred electrons = 2 in case of Cu^{2+} ions.

$(\Delta i)_m$ the maximum decrease in the limiting current density, corresponding to full surface coverage.

η the absolute viscosity of solution, $g \cdot cm^{-1} \cdot s^{-1}$.

θ the degree of surface coverage.

ρ^0 the density of bulk solution, g/cm^3 .

ρ^i the density of the solution at the interface, g/cm^3 .

$\Delta\rho = \rho^0 - \rho^i$, g/cm^3 .

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SUMMARY

Summary

The thesis deals with the study of the effect of the SAS on the electrodeposition process in acidified CuSO_4 solution and includes three chapters

The first chapter presents a survey on the mass transfer processes, types and shapes of electrodes, and literatures survey on previous work.

The second chapter is devoted for the results change of volt with current obtained by above measurements in absence and in presence of SAS with different concentrations and at different temperatures for cell using copper and lead anodes. The limiting currents, i_l , and the thermodynamic parameters (ΔF , ΔG° , ΔH° , ΔS°) were calculated.

The third chapter also discusses these results. It was found that Langmuir isotherm was applied and the adsorption parameters were calculated which were found to obey Langmuir adsorption isotherm. Data showed that the addition of SAS decrease the limiting current, and the decrease in limiting current is ranged from 5.7% to 26% for cell using copper anode and from 11.11% to 50% in the case of cell using lead anode depending on the nature of SAS and its concentration and alcohol. It is suggested that the decrease in the limiting current is attributed to adsorption of acid on the copper

surface and increases in the viscosity of the medium as well as the decrease in the diffusivity of Cu^{++} .

It was observed that the inhibitive efficiency of SAS in case of copper anode is in the order:

$$\text{CTAB} > \text{Triton X-100} > \text{SDS}$$

It was found that the inhibitive efficiency of SAS in case of lead anode is in the order:

$$\text{CTAB} > \text{Triton X-100} > \text{SDS}$$

and in the case of mixed SAS the order is as follow:

$$\text{SDS} + \text{CTAB} > \text{CTAB} + \text{Triton X-100} > \text{SDS} + \text{Triton X-100}$$

and in the case of alcohol the order is:

$$\text{Pentanol} > \text{Propanol} > \text{Ethanol} > \text{Methanol}$$

It was observed that the percentage of inhibition is lower in case of copper anode than in case of lead anode.

The thermodynamic results led to conclude that the rate of adsorption of these SAS was decreased by raising the temperature while above 30°C the desorption was complete indicating that the process is physical adsorption. The negative ΔS values suggest that the organic molecules are ordered in the solution under investigation.